

HIGH ENERGY STORAGE CAPACITY LOW COST IRON FLOW BATTERY

DEVELOPING A SLURRY ELECTRODE

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ALL-IRON FLOW BATTERIES:

- Single, low-cost active element - Iron
- Mild pH, non-toxic electrolyte
- Able to operate with inexpensive microporous separators
- **Iron is readily available domestically**
- Positive: $2Fe^{2+} \xrightarrow{\text{charge}} 2Fe^{3+} + 2e^-$ $E^0 = +0.77V$ vs NHE
- Negative: $Fe^{2+} + 2e^- \xrightarrow{\text{charge}} Fe^0$ $E^0 = -0.44V$ vs NHE

SLURRY ELECTRODES:

- Slurries are made by mixing conductive particles into the electrolyte.
- While charging, iron is plated onto the particles
- The particles carry the plated iron out of the active cell and are stored externally
- **Decouples power and energy capacity**

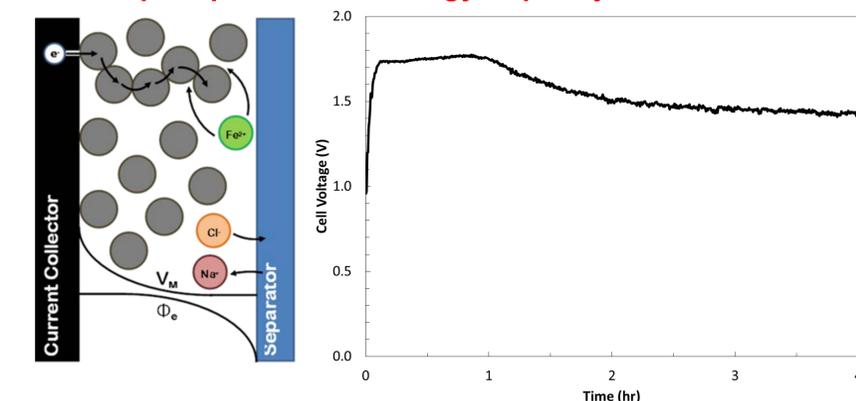


Figure 1: Cell voltage during initial charge at 200 mA/cm². Metalizing the carbon reduces the overpotential.

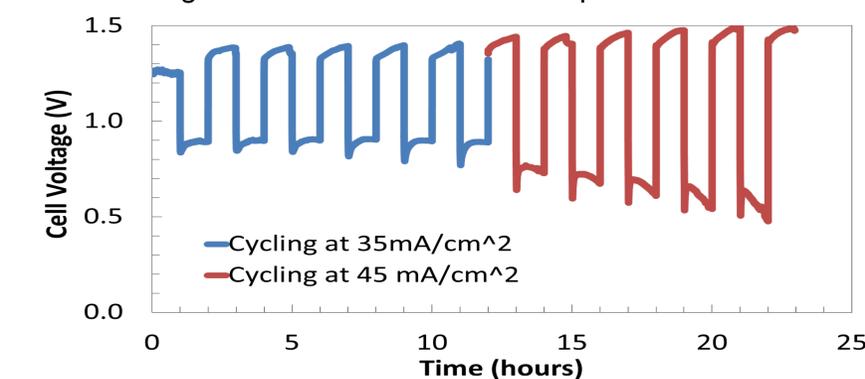


Figure 2: Cell voltage while cycling

GOALS OF THE ARPA-E PROGRAM:

- Optimize slurry electrode
 - Slurry stability, viscosity, conductivity
- Demonstrate operating prototype slurry electrode
 - Voltaic and coulombic efficiencies
- Model full scale stacks to estimate system performance
- **Develop strategic partnerships with expertise for scale-up, manufacturing, supply chain development, system integration, and testing**

RESULTS OF THE ARPA-E ONE YEAR SEED PROGRAM:

- Cost: \$105/kW and \$26/kWh
 - Achievable at 0.2 A/cm² and \$700/st Carbon
- Demonstrated stable, conductive, shear thinning slurries
- Parasitic losses due to pumping losses and shunt currents are < 2% for a 7 kW – 30 cell stack
- Negative Electrode Overpotential <100mV at 200 mA/cm² on charge
- Plating Capacity of >350 mAh Fe / g carbon feasible without loss of slurry stability

FUTURE WORK:

- Increase the electronic conductivity to promote more favorable current distribution and lower ohmic overpotentials
- Utilize more cost effective particles
- Scale and test 400 cm² prototype cell

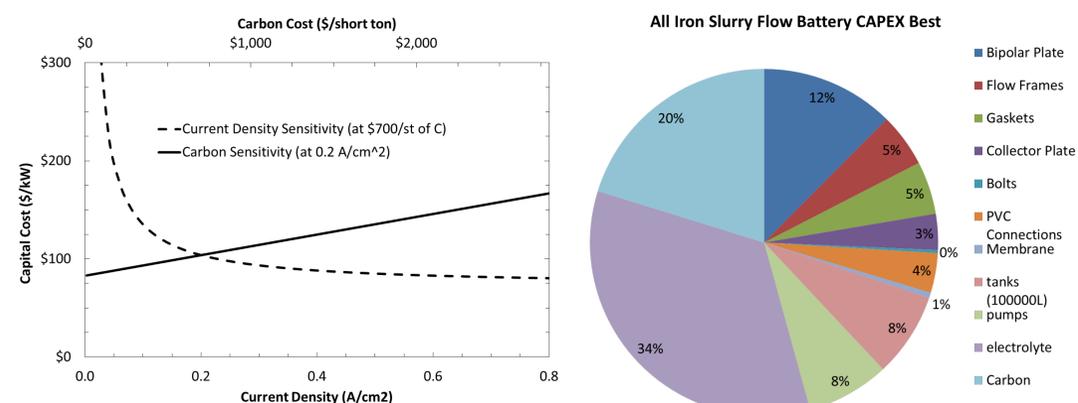


Figure 3: Estimated capital cost of a 1 MW / 4 MWh all-iron battery with slurry electrodes on both sides.

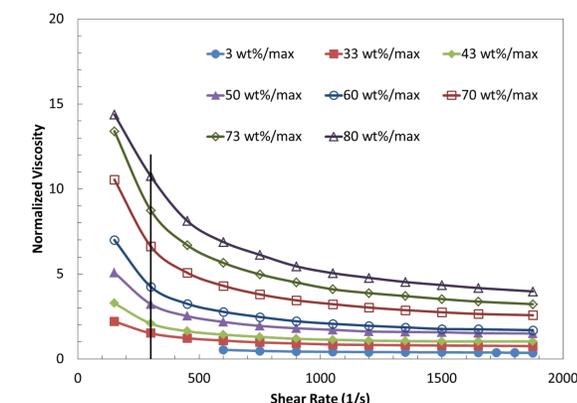
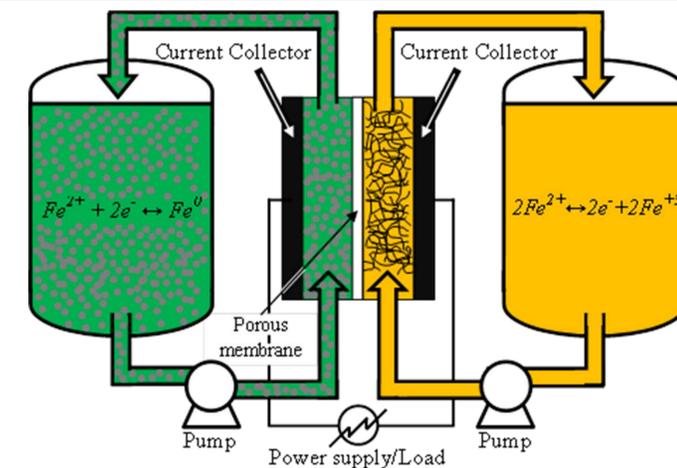


Figure 4: Slurry viscosity normalized to base electrolyte. The slurry shows shear thinning behavior. Typical shear is between 300-1200 s⁻¹.

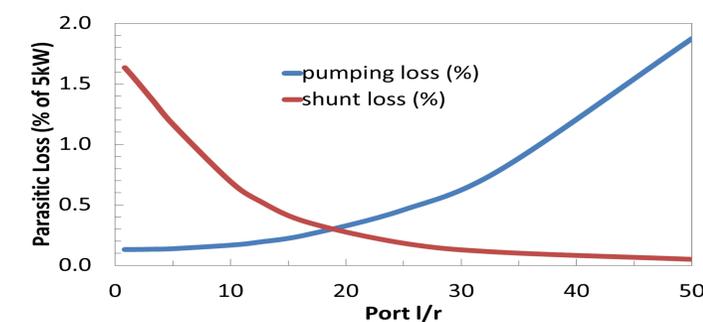


Figure 5: Shunt current and pumping losses. Model of a 30 cell stack, each 1000 cm². Stack power ≈ 5 kW at 140 mA/cm².

ACKNOWLEDGEMENTS

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