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# THERMAL RUNAWAY AT SCALE: ANALYZING ESS SAFETY WITH MODULE TO RACK SCALE MODELS

June 2-4, 2026

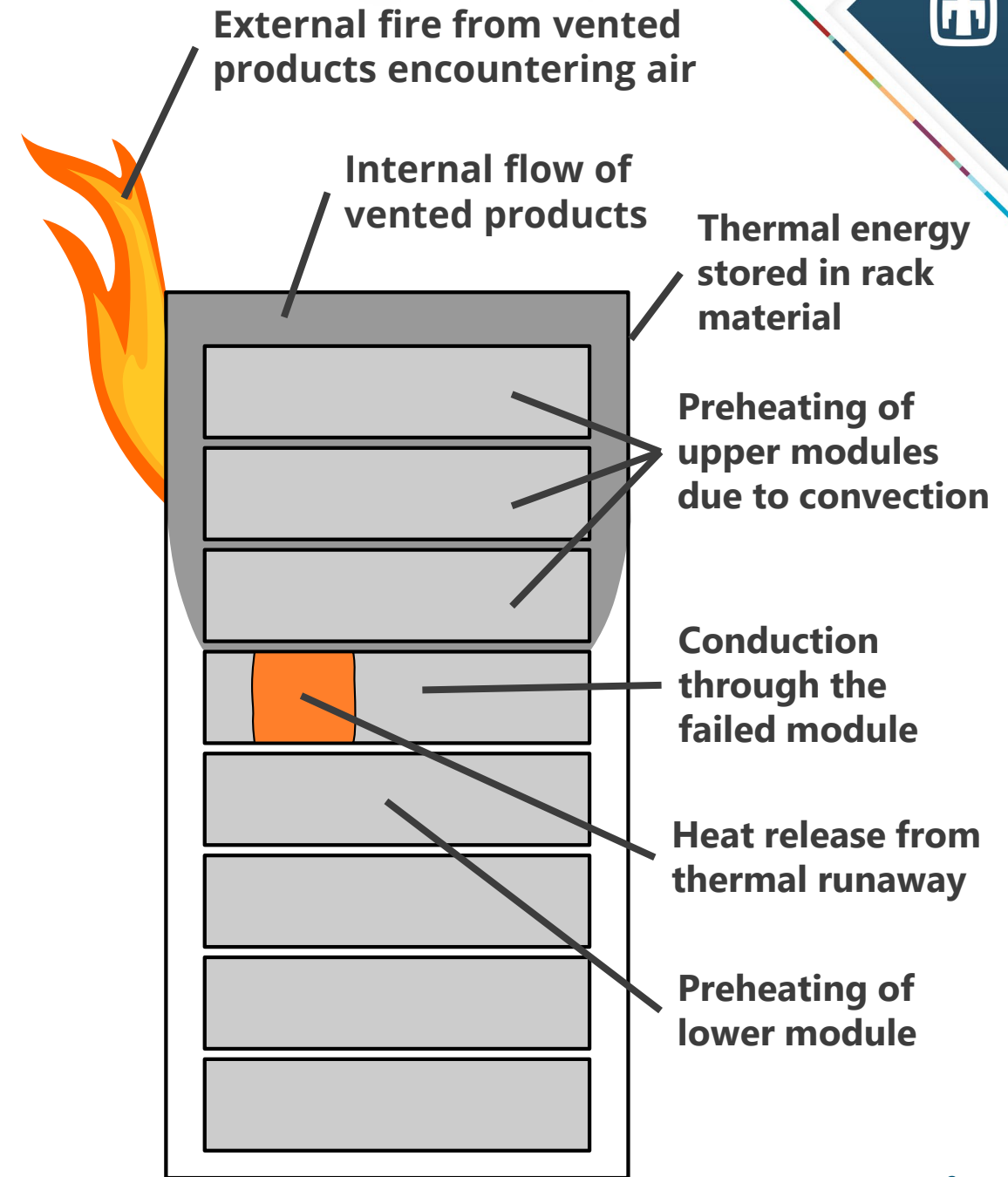
Andrew Kurzawski, Michael Meehan, Randy Shurtz,  
Loraine Torres-Castro, John Hewson

Energy Storage Safety and Reliability Forum

Albuquerque, NM

# THERMAL RUNAWAY MODELING

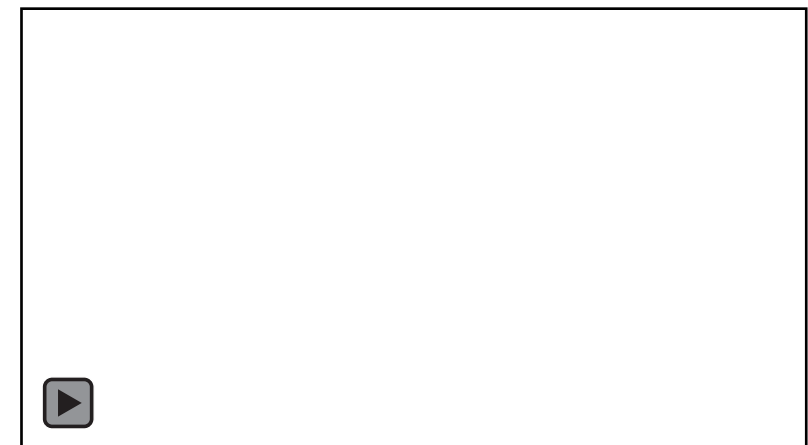
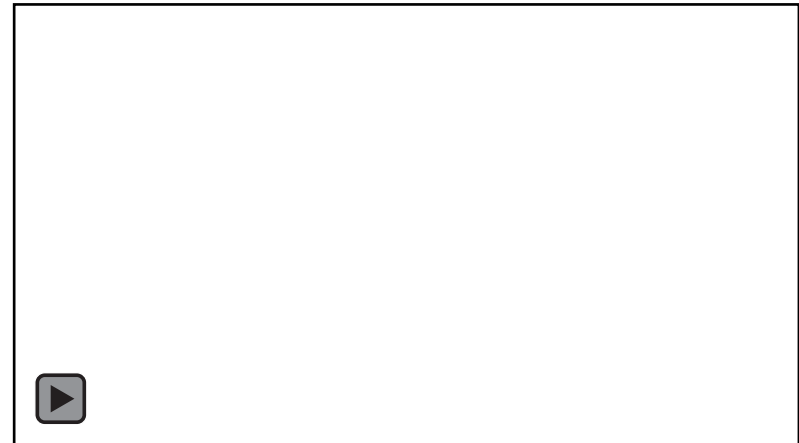
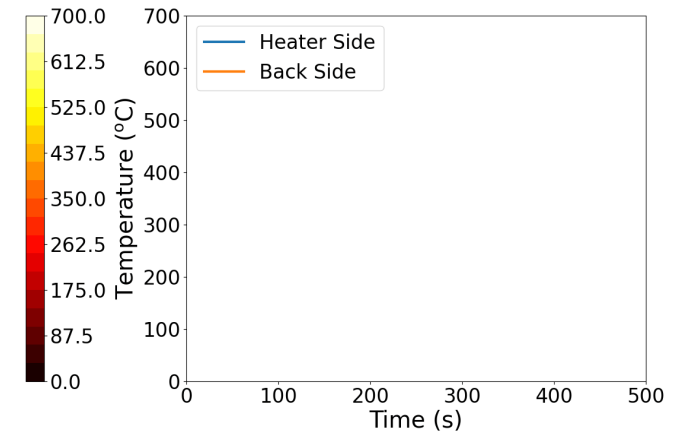
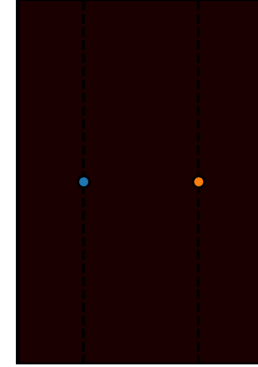
- Rich history of cell-level thermal runaway modeling dating back over 20 years
- Applying these models at larger (module/rack) scales presents additional challenges
- Scale of problem can be defined by heat transfer:
  - Fast: internal cell heating
  - Medium: cell-to-cell heat transfer
  - Slow: module-to-module interactions
- How can models improve our understanding of system-level safety?



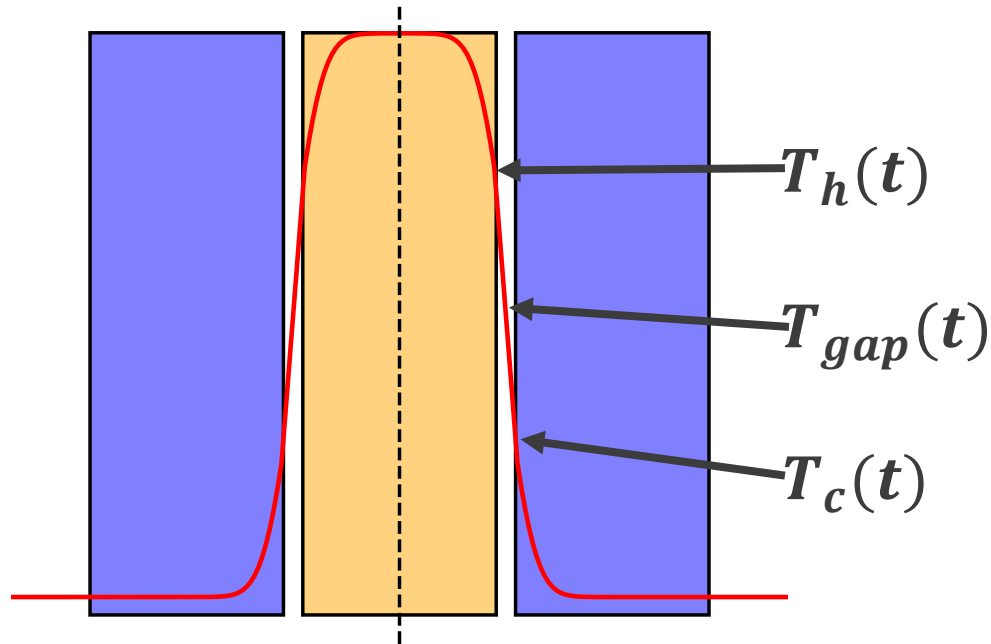
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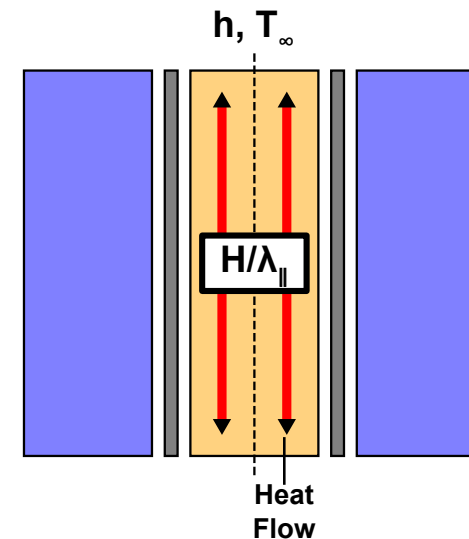
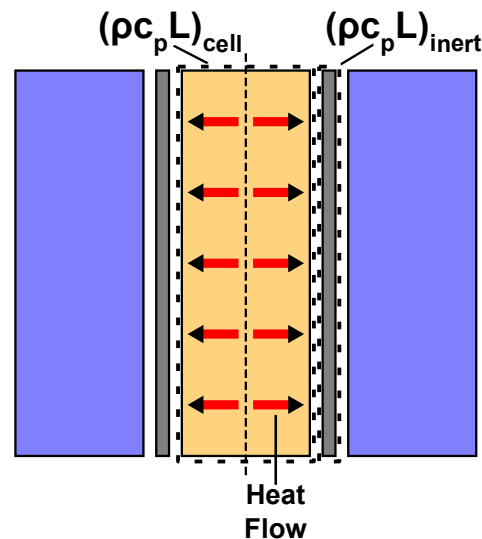
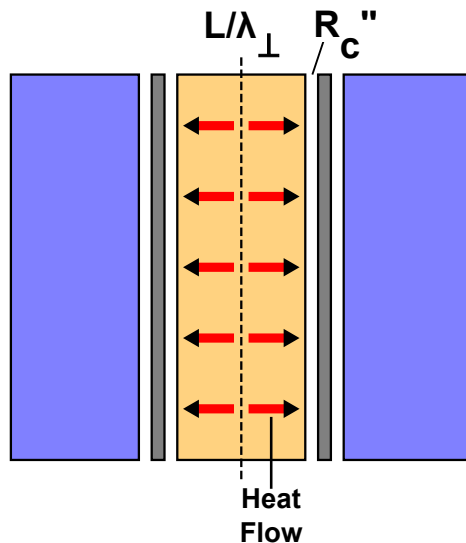
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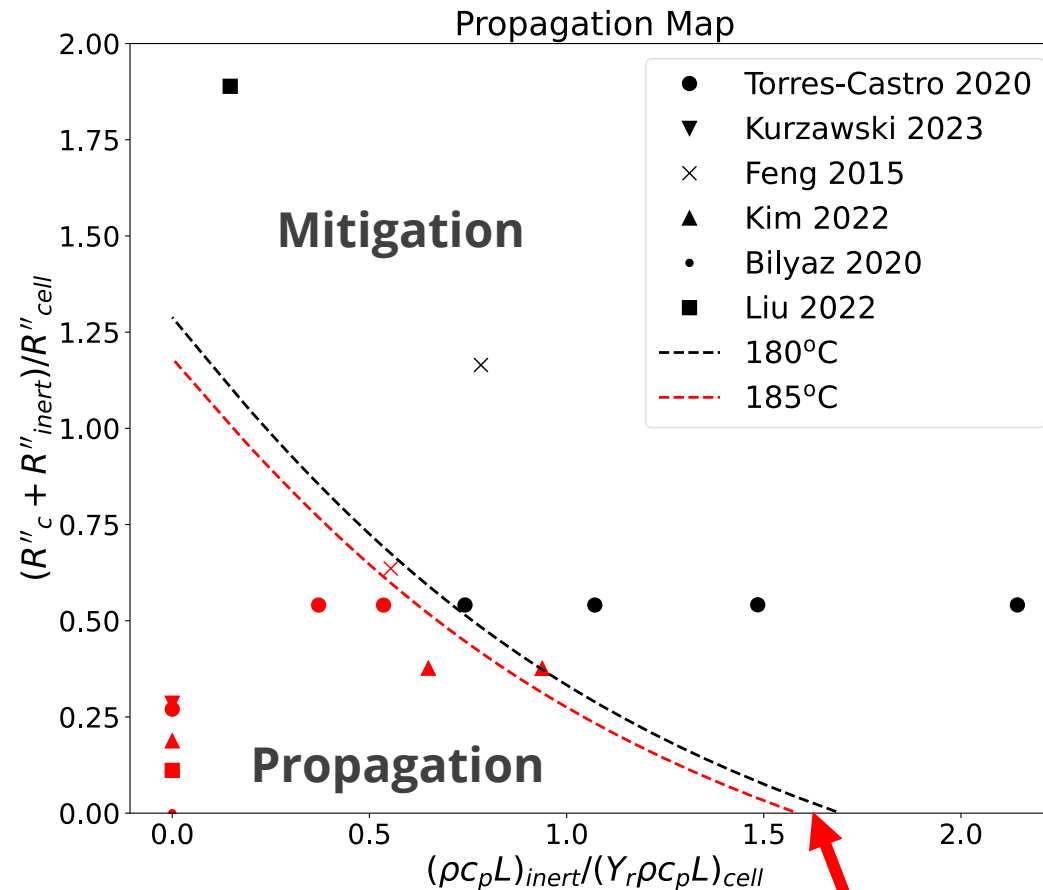
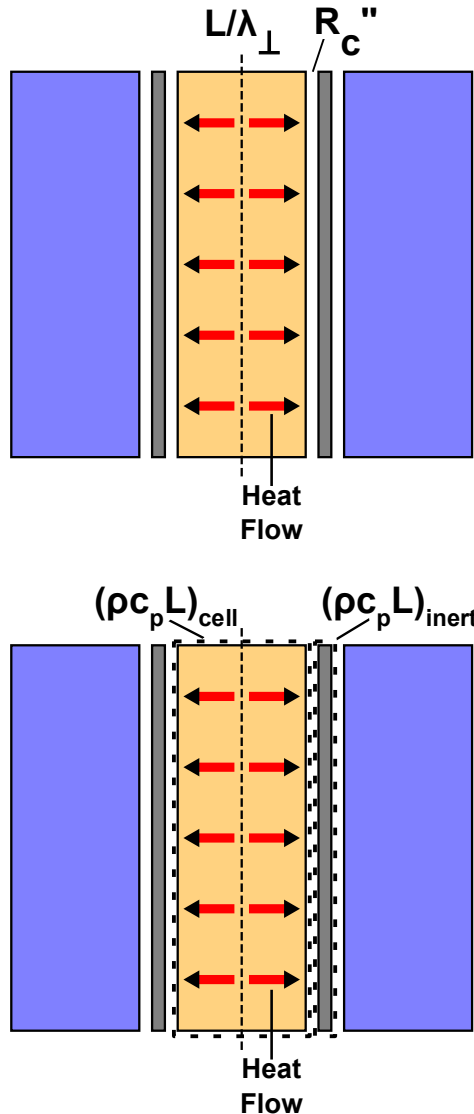
# CELL-TO-CELL SCALE PROPAGATION/MITIGATION REGIMES



- Simple model focusing on heat transfer between two cells
- Three non-dimensional parameters can be used to describe heat transfer
  - Conduction resistance
  - Heat capacity ratio
  - External losses
- Thermal runaway assumed when  $T_c > T_{onset}$



# CELL-TO-CELL SCALE PROPAGATION/MITIGATION REGIMES



## Key features

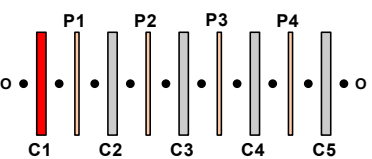
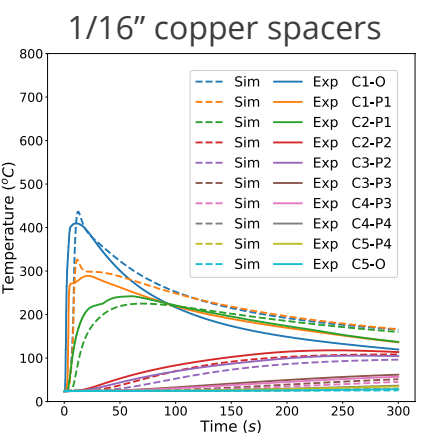
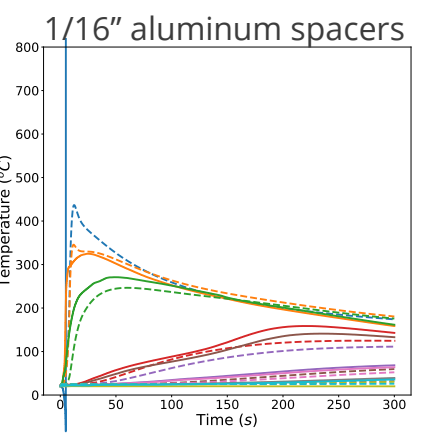
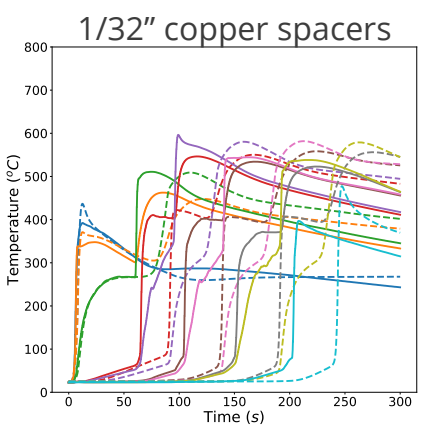
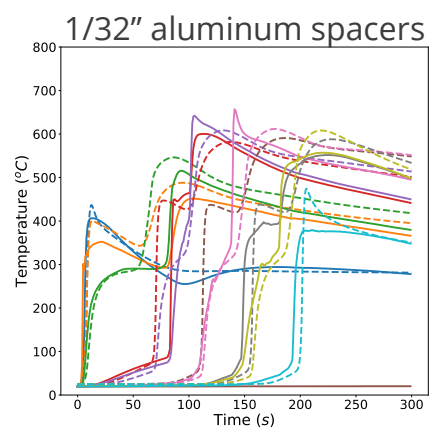
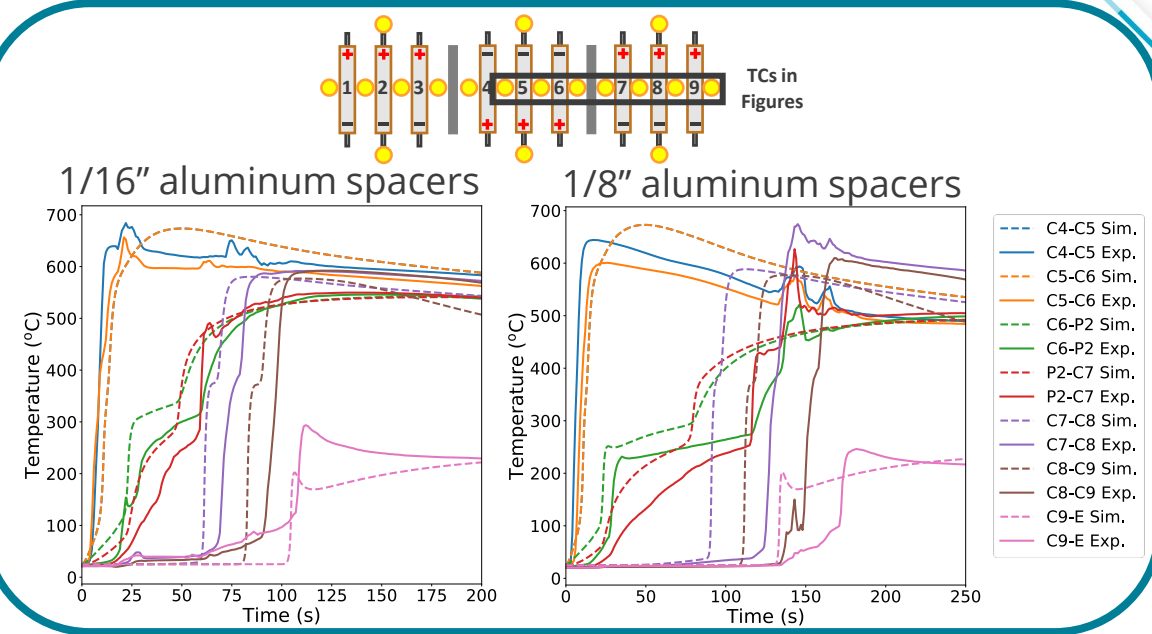
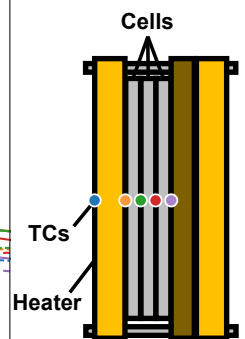
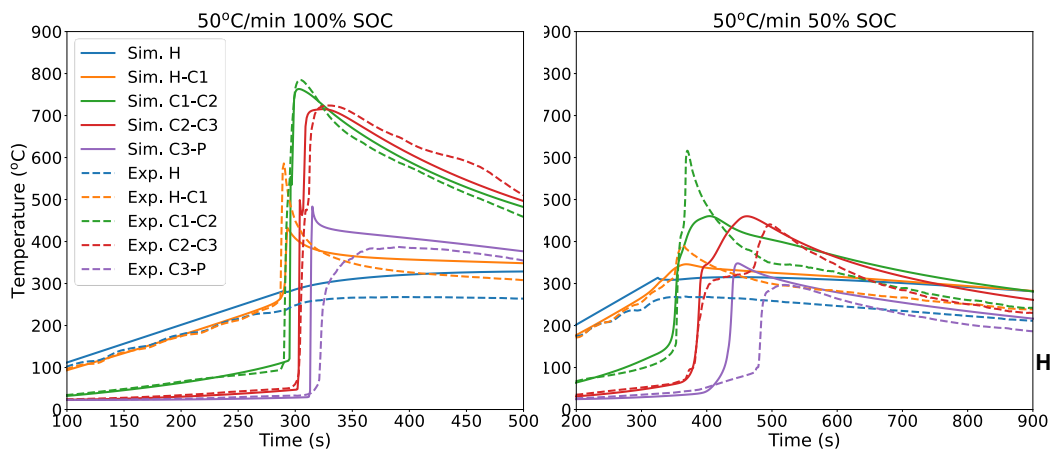
- Assume losses to ambient
- Range of cell sizes with different inter-cell materials
- Vertical axis: ratio of inter-cell resistance to internal resistance
- Horizontal axis: ratio of intercell heat capacity to heat capacity remaining in cell after venting

## Main uncertainties

- Mass loss
- Contact resistance



# VALIDATION OF PROPAGATION/MITIGATION



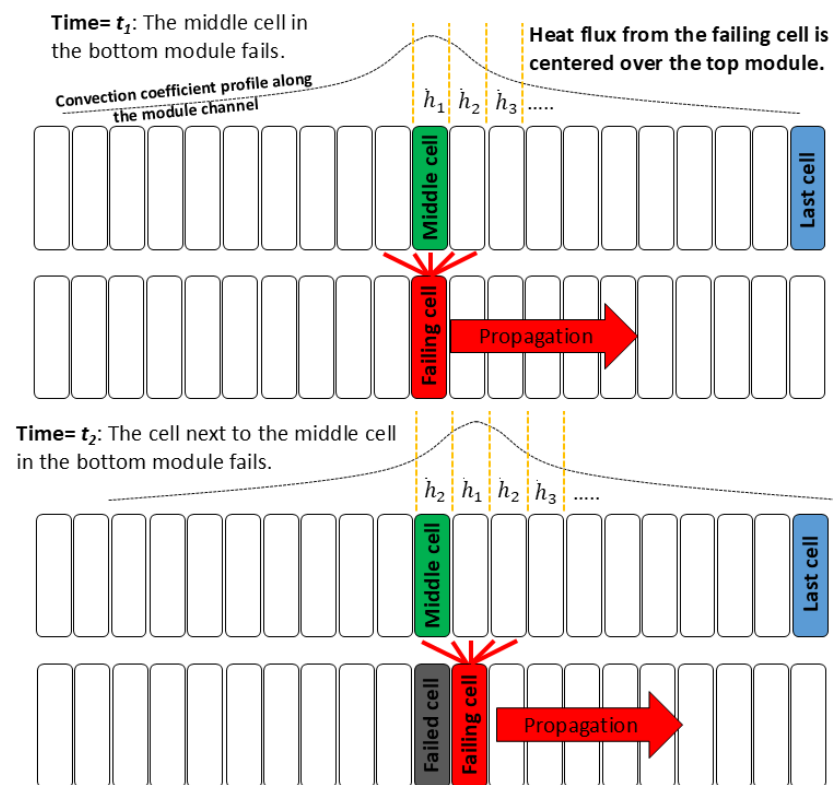


# VENT GAS HEAT TRANSFER

- Li-ion batteries undergoing thermal runaway produce hot combustible gases and solid particles that can heat other cells in the system
- Gases impinge directly on the surface above and travel through channels between modules, heating more distant cells.
- Heating from successive failures spreads heat through the system.



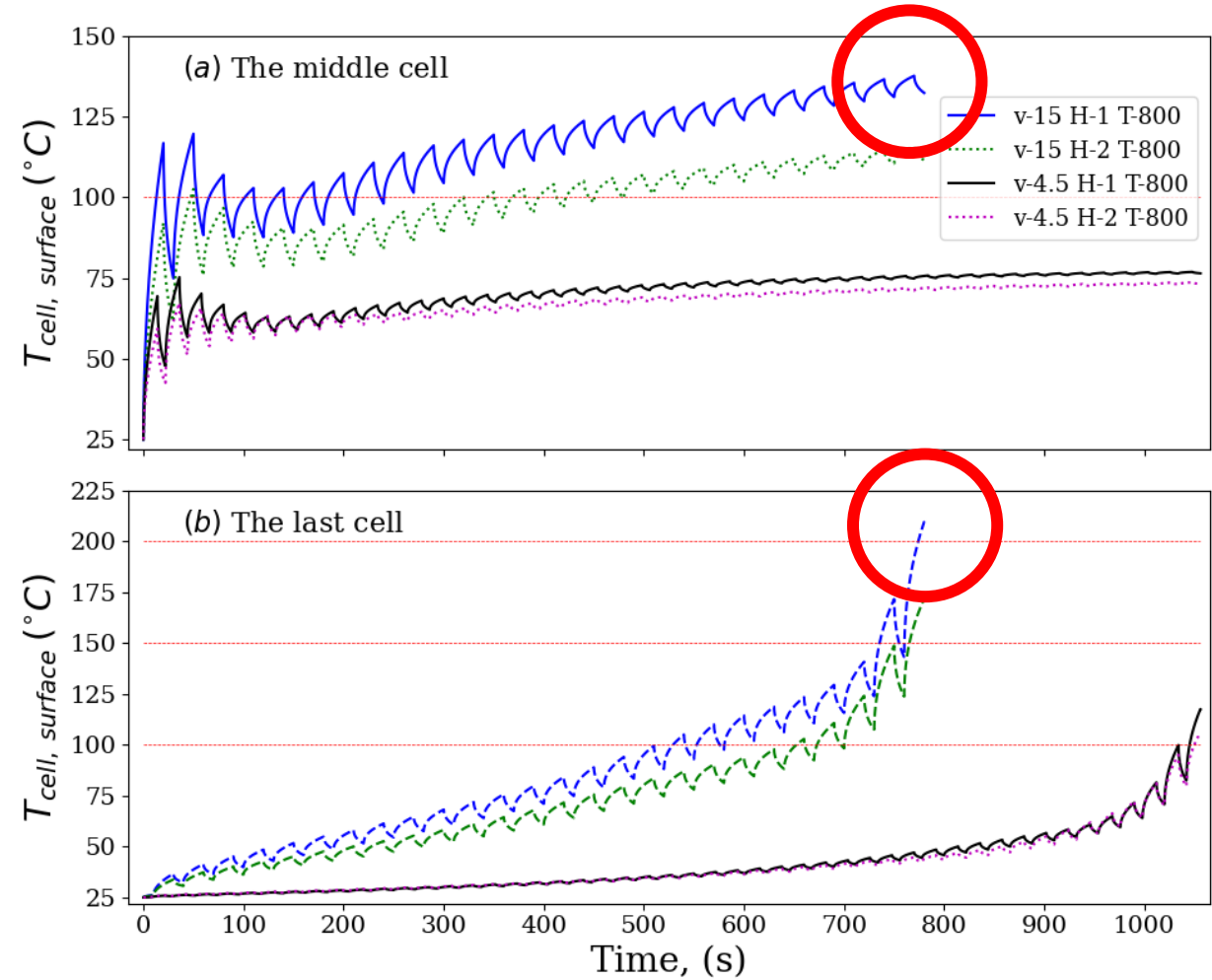
Example vent impingement



Lower module to upper module heat transfer from successive vents

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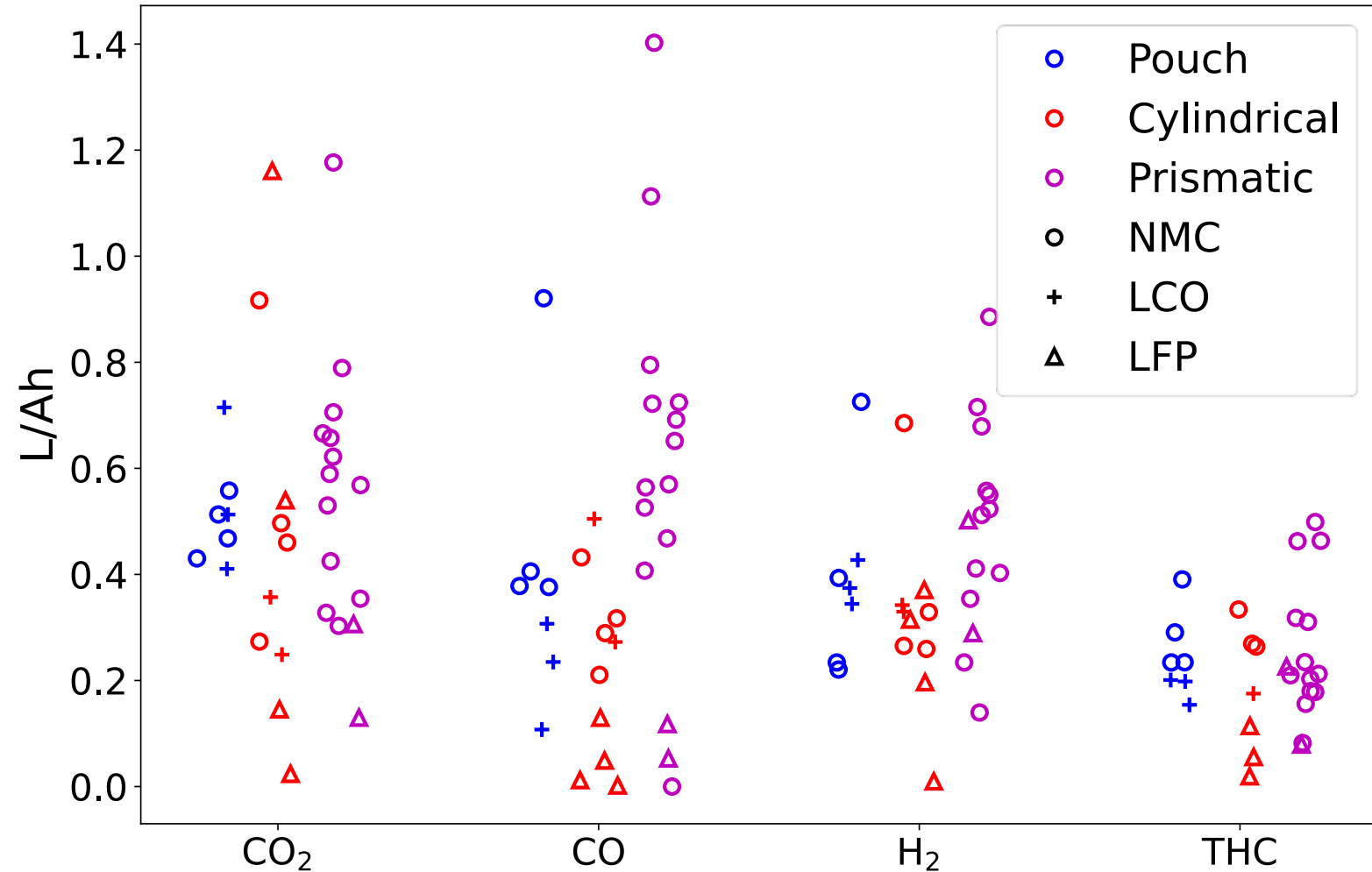


**Preheating of the last cell of the upper module results in higher temperatures**

# VENT GAS COMPOSITION: LITERATURE DATA

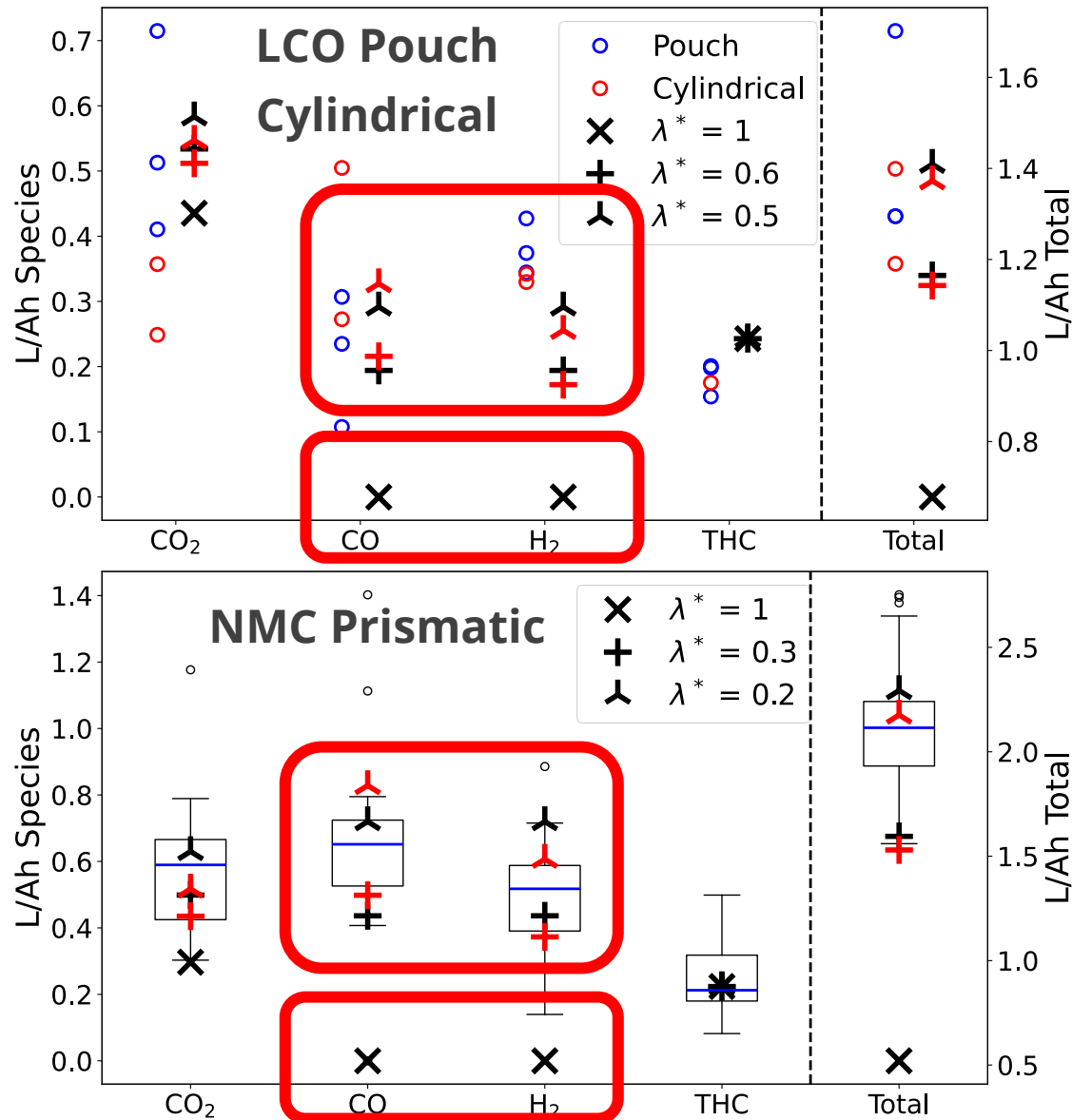
- The vent gas is primarily composed of CO<sub>2</sub>, CO, H<sub>2</sub>, and hydrocarbons.
- The flammable gases can burn or pose explosion/deflagration hazard.
- Recent studies (Baird et al. 2020 and Bugryniec et al. 2024) have aggregated data from multiple sources.
- A large amount of variability exists in the data even between replicates in the same study.

100% SOC cells in inert environments with different abuse methods



Data from Bugryniec et al. 2024 <https://doi.org/10.1016/j.est.2024.111288>

# VENT GAS COMPOSITION: MODELING

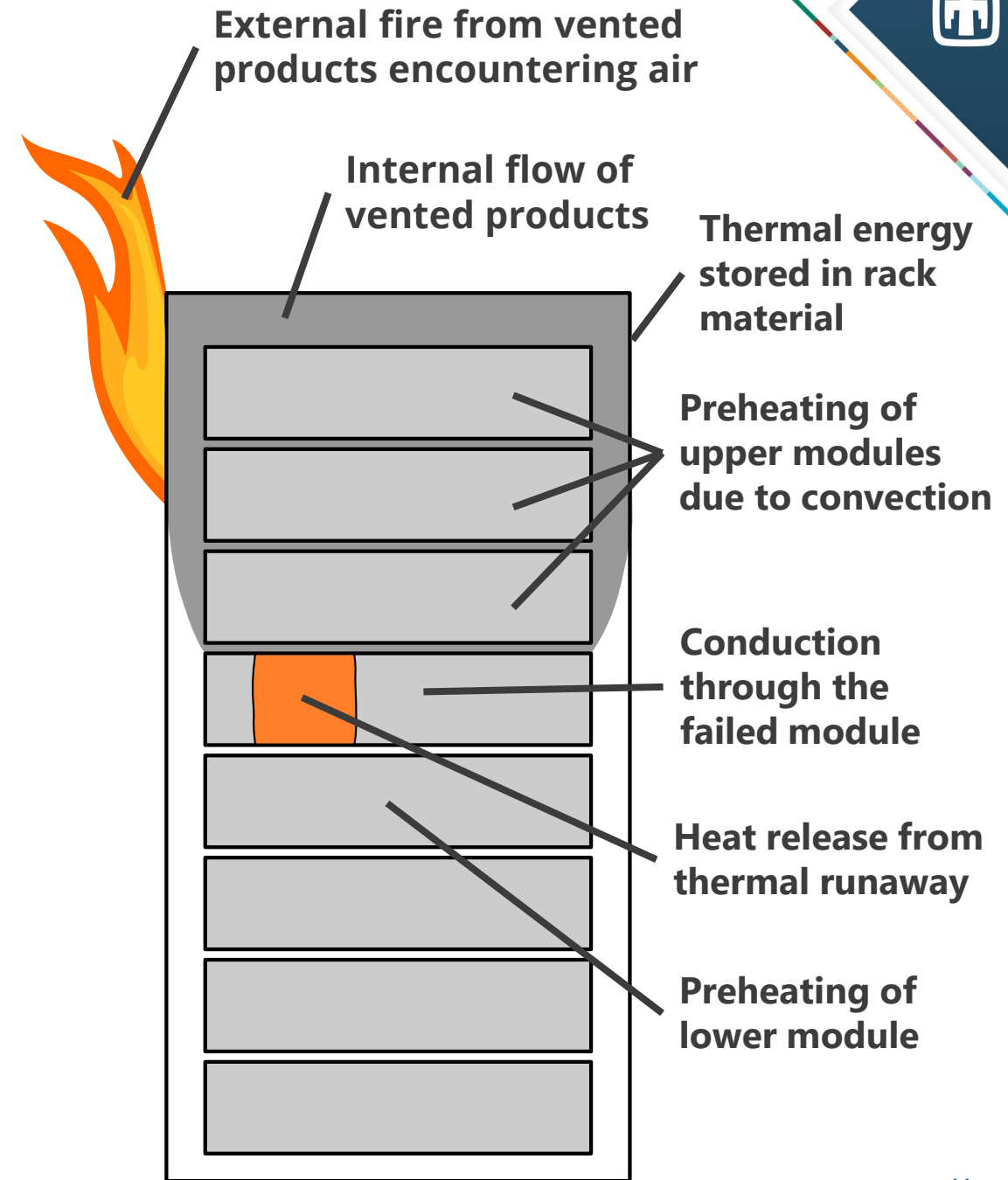


- Modeled thermal runaway and gas production for two example cells in LIM1TR software.
- Full oxidation of ethylene carbonate (EC) only produces CO<sub>2</sub> and water vapor.
 
$$5\text{MO}_2 + (\text{CH}_2\text{O})_2\text{CO} \rightarrow 5\text{MO} + 3\text{CO}_2 + 2\text{H}_2\text{O}$$
- Partial oxidation of EC
 
$$5\text{MO}_2 + \phi(\text{CH}_2\text{O})_2\text{CO} \rightarrow 5\text{MO} + a\text{CO}_2 + b\text{CO} + c\text{H}_2\text{O} + d\text{H}_2$$
- Two closure methods for partial oxidation: linear closure (black symbols) and water-gas shift closure (red symbols).
- The inclusion of cathode partial oxidation improves gas predictions, and ongoing work is focused on contributions from the anode.

# HEAT TRANSFER AT THE RACK SCALE

Modeling challenges at the rack scale:

- **Variability in design:** enclosed/open shelves, presence of wiring, ventilation pathways, passive/active cooling.
- **Uncertainties:** thermal contact resistances, cell heat release, dynamical ventilation pathways, pressure loss coefficients for gas accumulation.
- **Multi-physics coupling:** turbulence, combustion, phase change (e.g., plastic/aluminum melting), chemistry.
- **Sparse availability of test data:** testing at these scales are dangerous, expensive, and generally involves proprietary information



# RACK MODEL

**Description:** 2-D sims with Sandia's Sierra/Fuego CFD code to simulate battery venting. A RANS turbulence model and EDC combustion model are used. Statistics are taken after flow becomes (statistically) stationary.

Parameter list:

- Module width: 80 cm
- Module height: 10 cm
- Opening width: 10 cm
- Channel height: 2 cm
- Vent width: 1 cm
- Vent velocities: 1, 2, ..., 25 m/s
- Vent module: 1, 3, 5
- Vent temperature: 800, 1200 K
- Air temperature: 300 K

Roughly equivalent to LFP pouch cell

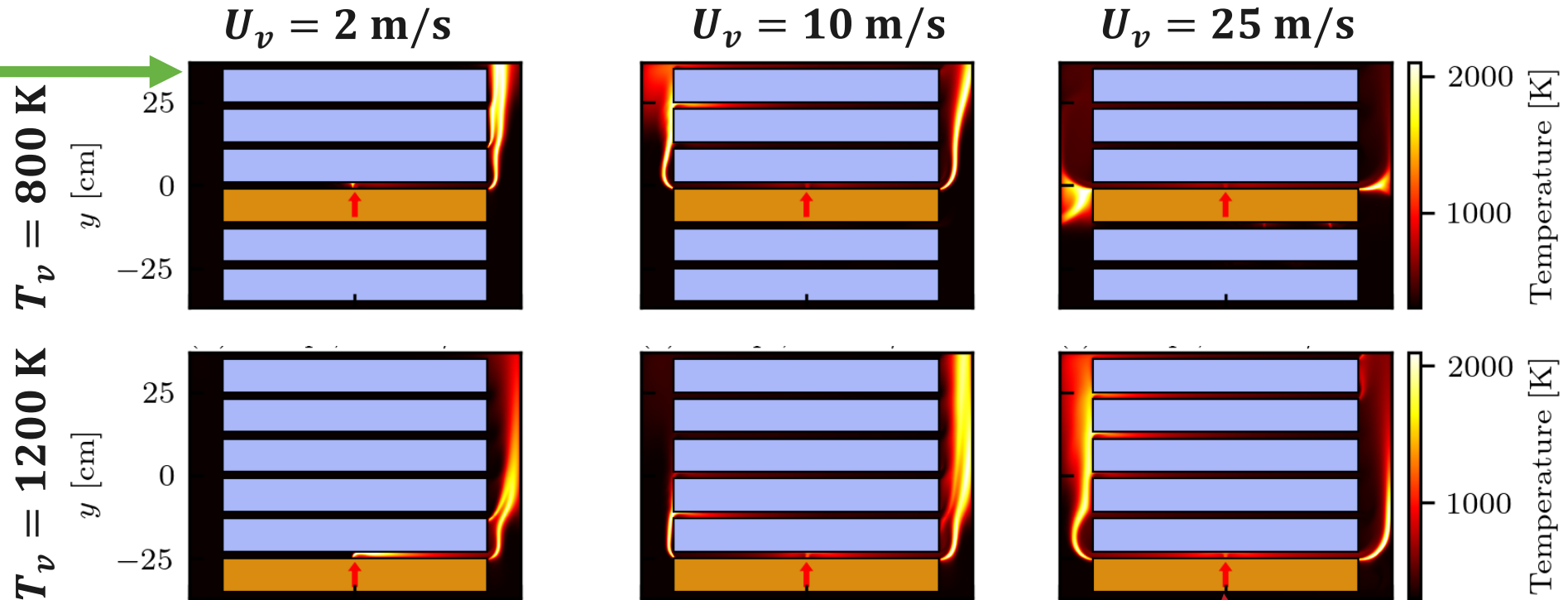


Figure showing time-average temperature fields for different vent velocities and temperatures

Approaching equivalence of NMC prismatic cell

# VENT GAS FLOW AND HEAT TRANSFER

## Key findings:

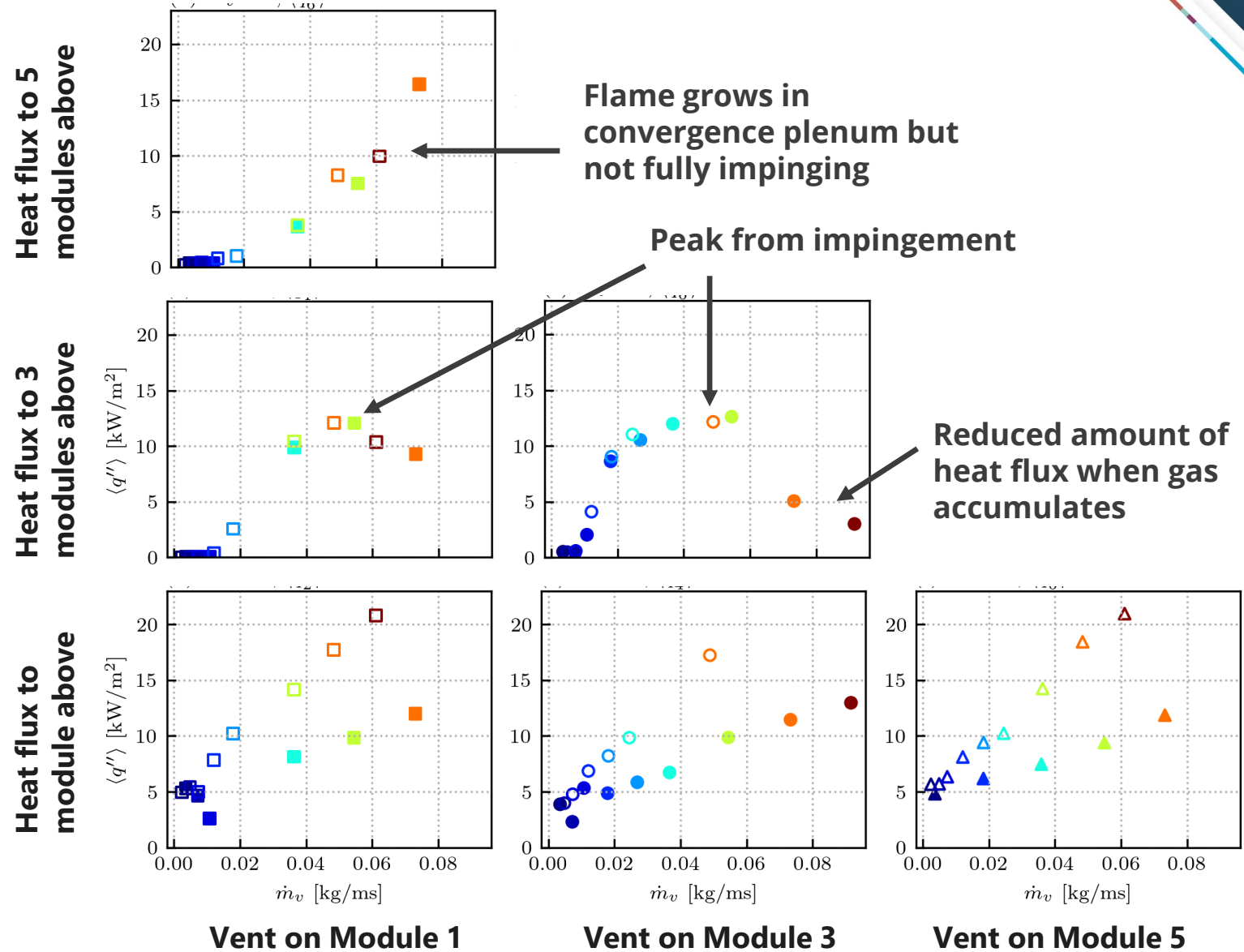
- Heat flux to the module above venting (bottom row) scales according to jet impingement physics
- Heat flux to non-adjacent modules peaks when flame impinges on the module and remains non-zero during hot gas accumulation.

### Legend for images

Color: blue to red = increasing velocity

Symbol: module number

Fill: open = higher vent temperature



# VENT GAS FLOW AND HEAT TRANSFER

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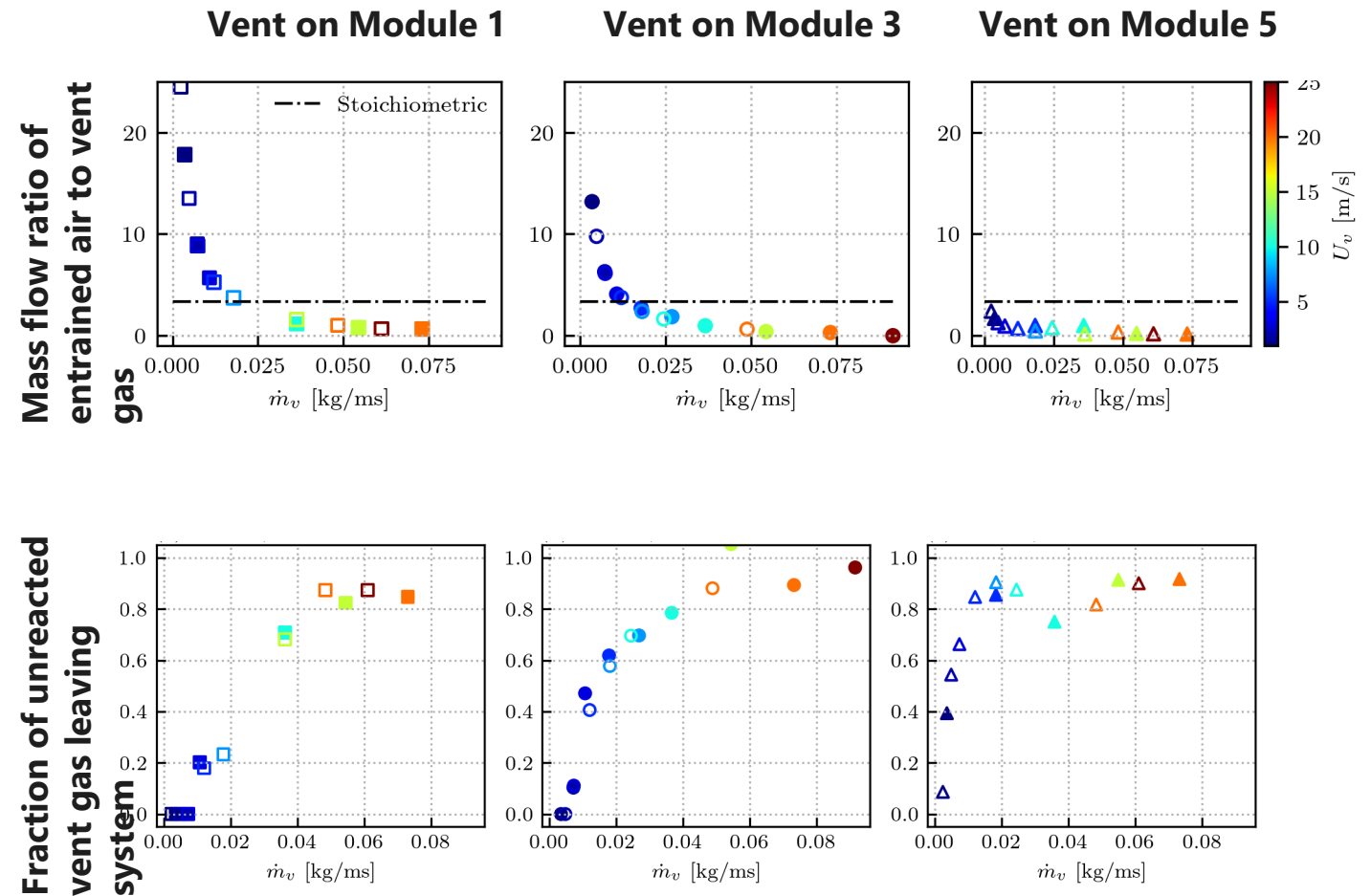
- More air entrainment when the vent is near the bottom and released slowly to generate large buoyant force relative to momentum
- Under most realistic conditions, vent gas leaves ESS unreacted. Resulting in heat release outside of rack endangering neighboring racks.
- Unreacted vent gases mixed with entrained air near stoichiometric conditions pose a greater ignition/deflagration hazard.

### Legend for images

Color: blue to red = increasing velocity

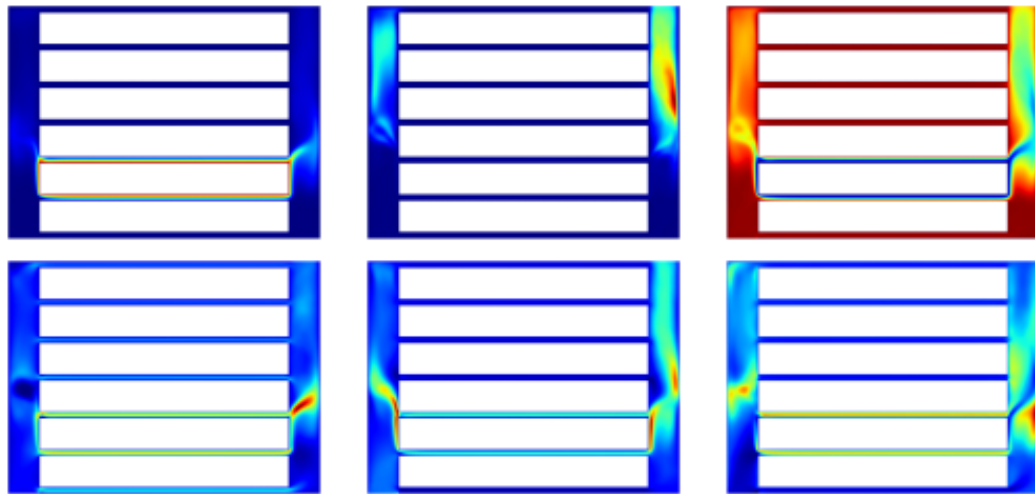
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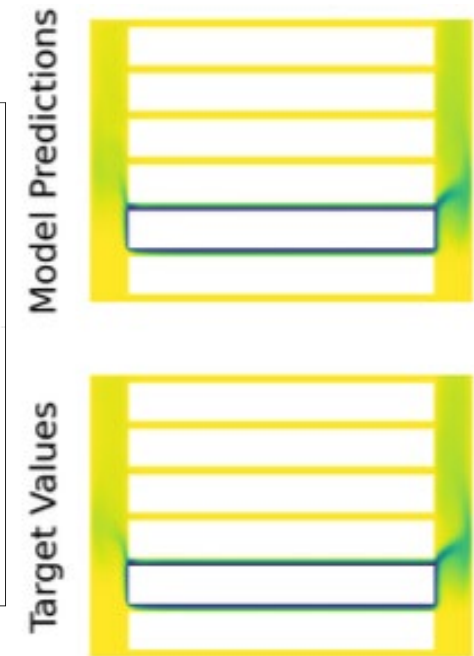
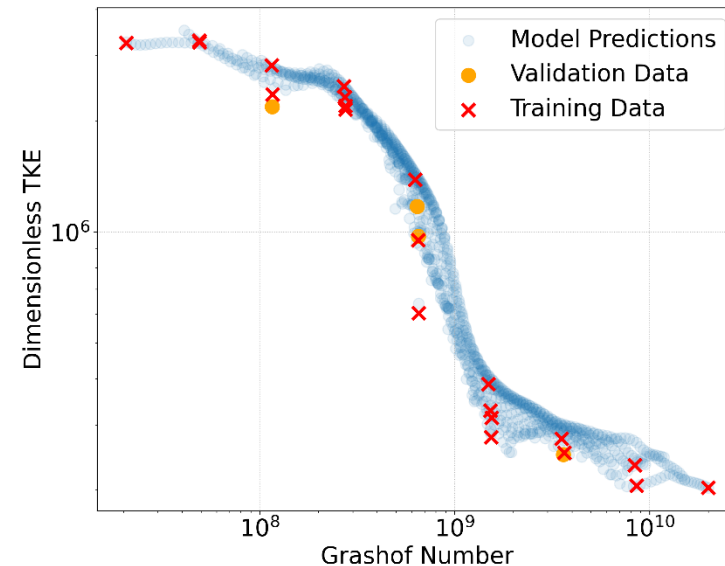


# MACHINE LEARNING APPROACH

- Use *structure-preserving* reduced-order modeling methods to *learn* a reduced finite element basis and a nonlinear conservation law using simulation data. Creates physics-conserving model by *construction*.
- The reduced-order model can:
  - Feedback into cell-to-cell propagation (e.g., heat flux)
  - Build control algorithms for active mitigation
  - Include physics-conserving properties by construction



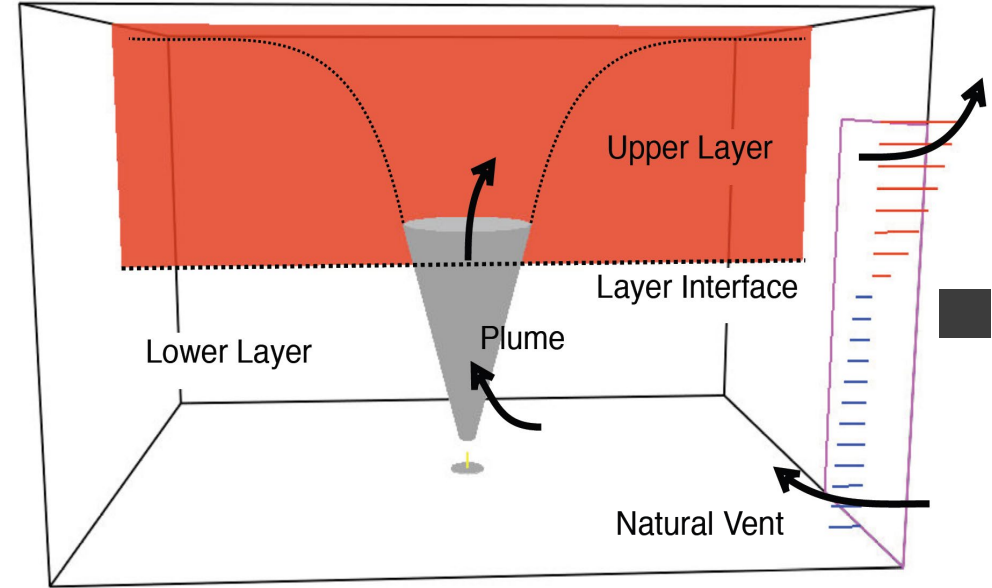
Reduce simulations of millions of elements to only 6 coarse elements, allows real-time evaluation speeds



Excellent accuracy shown using turbulent kinetic energy (heat transfer, left) and field reconstructions (right)

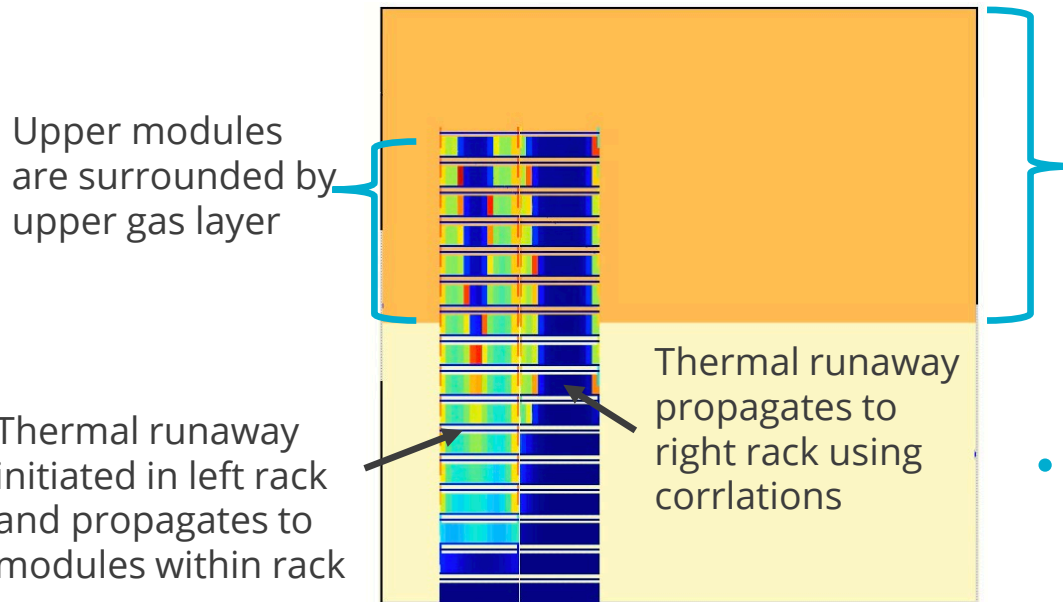
# HEAT TRANSFER BEYOND THE ORIGINATING RACK

- CFD at the room scale is computationally expensive, inhibiting exploration of large parameter spaces
- Correlations and network models offer means of exploring parameters, but these models need inputs from the rack scale models



→ Components of mass and enthalpy entering or leaving a control volume

*\*Source: CFAST Technical Reference Guide Version 7*

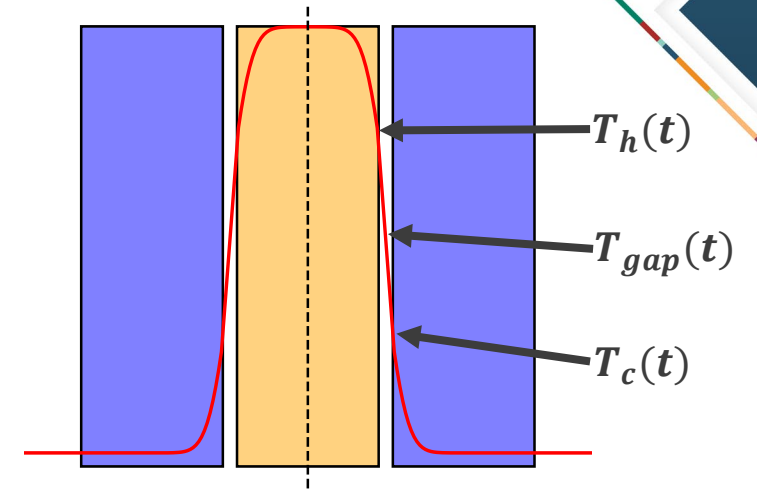


Upper gas layer size is dictated by cell level gas composition and release rate within rack(s)

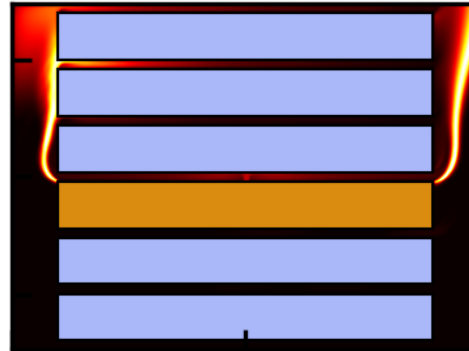
- Continuation of testing campaigns better grounds models in physical reality

## SUMMARY

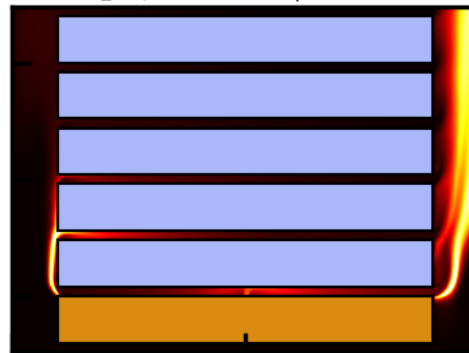
- A range of modeling tools are needed to predict thermal runaway at different scales.
- Models feed into each other, from cell-level heat and gas release up to room-scale fire effects.
- We seek to balance accuracy and computational complexity to explore a range of scenarios while validating predictions against along the way.



Temp., T800/U750



Temp., T1200/U750





# ACKNOWLEDGEMENTS

This material is based upon work supported by the U.S. Department of Energy, Office of Electricity (OE), Energy Storage Division.

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